



# OXIDATIVE COUPLING OF METHANE PERFORMANCE IN A NOVEL MEMBRANE REACTOR

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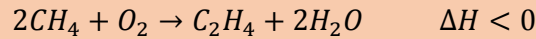


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## Introduction

The oxidative coupling of methane (OCM) is a direct route for the production of hydrocarbons (C<sub>2+</sub>) from methane.



The OCM yield is hampered by the parallel oxidation reactions, and at least a 30% C<sub>2+</sub> yield is needed to make the process economically viable.

## Packed bed reactor

The exothermic behaviour of the OCM results in a heat management issue that needs to be solved. In a packed bed reactor, a controlled temperature regime results in a very poor C<sub>2</sub> yield.

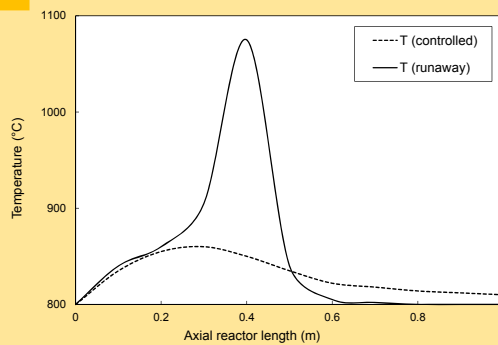


Figure 1. OCM Temperature profiles along the axial reactor length of a packed bed reactor.

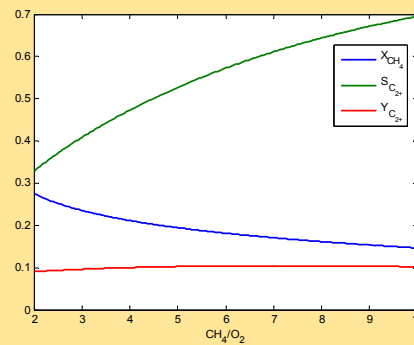


Figure 2. OCM performance for different CH<sub>4</sub>/O<sub>2</sub> ratios with a conventional configuration.

Very poor performances are achieved with conventional configurations (when CH<sub>4</sub> and O<sub>2</sub> are co-fed).

Optimization of the catalyst used for the process

## To improve the OCM performance...

Improve reactor design

Mn-Na<sub>2</sub>WO<sub>4</sub>/SiO<sub>2</sub>, one of the most promising OCM catalysts, has been selected to perform the experiments. The main findings are the following:

- S<sub>C<sub>2</sub></sub> above 50% in membrane reactor conditions.
- Stable under OCM conditions (800 °C and 2 bar) for 100 operating hours.
- C<sub>2</sub>H<sub>6</sub> → C<sub>2</sub>H<sub>4</sub> + H<sub>2</sub> main route for the C<sub>2</sub>H<sub>4</sub> production.
- C<sub>2</sub>H<sub>4</sub> + 3 O<sub>2</sub> → 2 CO<sub>2</sub> + 2 H<sub>2</sub>O } Most important undesired 2<sup>ary</sup> reactions. Minimization of these fast reactions is crucial to obtain a good OCM performance.
- C<sub>2</sub>H<sub>4</sub> + O<sub>2</sub> → 2 CO + 2 H<sub>2</sub>
- Use of catalyst increase the velocity of the 2<sup>ary</sup> reactions, thus faster consuming the C<sub>2</sub> formed in previous steps.

## Packed bed Membrane Reactor

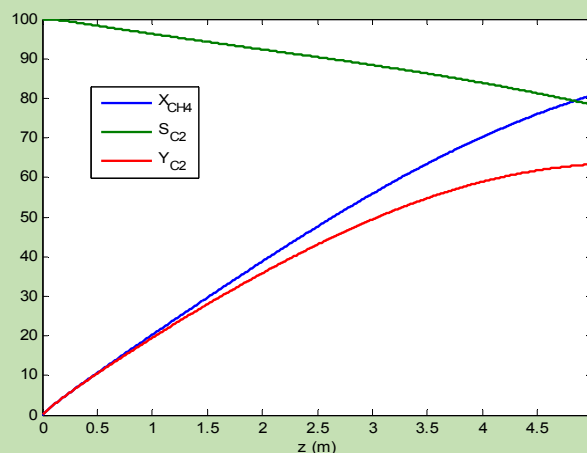


Figure 3. OCM performance along the axial length of a packed bed membrane reactor.

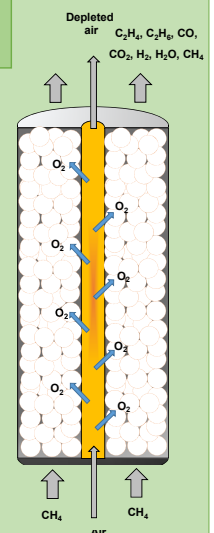


Figure 4. Scheme of an OCM packed bed membrane reactor.

## Conclusions

- The yield obtained with the conventional configuration (packed bed) is not enough to make the process economically viable.
- The utilization of the Mn-Na<sub>2</sub>WO<sub>4</sub>/SiO<sub>2</sub> catalyst together with the OCM membrane reactor configuration can contribute to reach the 30% C<sub>2</sub> yield required to make the process competitive with other ethylene production technologies.

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